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Complete List of Authors:	Ramesh, G.K.; Presidency University, Bengaluru, Mathematics Kumar, K.; Kuvempu University Shehzad, S.A.; COMSATS Institute of Information Technology, Mathematics Gireesha, B.J.; Kuvempu University
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Enhancement of radiation on hydromagnetic Casson fluid flow towards a stretched cylinder with suspension of liquid-particles

G.K.Ramesh^{1*}, K.Ganesh Kumar², S.A.Shehzad³ and B.J.Gireesha²

¹Department of Mathematics, School of Engineering, Presidency University,
Yelahanka, Bengaluru-560089, Karnataka, India

²Department of Studies and Research in Mathematics, Kuvempu University,
Shankaraghatta-577 451, Shimoga, Karnataka, India.

³Department of Mathematics, COMSATS Institute of Information Technology,
Sahiwal 57000, Pakistan

*Corresponding author email-id: gkrmaths@gmail.com (G.K.Ramesh) Ph: +91 9900981204

Abstract: The presence of dust particles is involved in many engineering and industrial processes like transport of petroleum, emission of smoke from vehicles, piping of power plants, treatment of waste-water and corrosive particles in mining. Due to such importance of this phenomenon, we considered the Casson liquid flow past a stretching hollow cylinder with fluid-particle suspension and convective boundary condition aspects. Numerical solution is obtained via shooting techniques after the applying of similarity variables to the governing partial equations. Key parameters of problem are discussed through graphs. It is noticed that the clean fluid temperature is always higher values as compared to dust fluid and also presence of radiation enhanced the temperature at the surface.

Keywords: Casson fluid, cylindrical surface, convective condition, nonlinear thermal radiation, liquid particle suspension.

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1. Introduction

The suspension of fluid-particles has major role in nature, science and technological applications. Few examples of such applications from our daily life may include paints, food products, biological liquids, pharmaceuticals etc. Further the investigations on mechanism of fluid-

particles submersion is a topic of hot interest nowadays because of its involvement in engineering and industry like in transport of petroleum, treatment of waste-water, emission of smoke from vehicles, piping of power plants and corrosive particles in mining. The deposition and transportation of particles is involved in different processes such as cool transport, cleaning, water and air pollution, xerography, combustion, filtration etc. [1]. Such practical implementation has engaged the researchers to elaborate the rheological features of suspension. For instance, Gireesha et al. [2] elaborated the nature of three-dimensional Couette fluid flow with suspension of liquid-particles. They computed the closed form expressions for the solution of problem. A molecular dynamic technique for the entropy generation in Couette flow with particles suspension has been described by Wang et al. [3]. Roopa et al. [4] explored the mechanism of fluid-particles submersion in time-dependent stretched surface. Manjunatha et al. [5] investigated the phenomenon of radiative heat transport in flow of dusty liquid under the aspects of heat generation. Abbas et al. [6] computed of two-phase liquid flow past through a channel. Sulochana and Sandeep [7] presented a research on the analysis of MHD viscous liquid flow with nano-particles and fluid-particles. Ramesh et al. [8-10] reported the two-phase dusty liquid flow over a permeably moving sheet under various aspects and conditions.

The consideration of boundary layer phenomenon of dusty non-Newtonian liquids with heat transport is very essential for better understanding of engineering and industrial technological problems like guided missiles rain erosion, fluidization, atmospheric fallout, lunar ash flows, paint and aerosol spraying, cooling of nuclear reactor etc. Here Casson liquid model is considered as a non-Newtonian fluid. This model is very popular amongst the recent investigators. Hayat et al. [11] addressed the convective condition role in hydrodynamic Casson liquid flow. Nonlinear radiative characteristics of Casson fluid induced by a wedge have been

numerically reported by Raju and Sandeep [12]. Hakeem et al. [13] described the features of inclined Lorentz force in Casson liquid flow induced by the moving permeable sheet. Numerical simulation for binary chemically reactive Casson liquid has been made by Abbas et al. [14]. Ramesh et al. [15] presented the numerical analysis of Casson fluid past a moving sheet with variable properties. The combined analysis of heat and mass diffusions in time-dependent Casson liquid induced by cone and flat plate has been reported by Benazir et al. [16]. They also addressed the features of double dispersion, porous medium and Joule heating in this article. Shehzad et al. [17] developed the three-dimensional flow model of Casson liquid in presence of porous media and heat generation. Rauf et al. [18] reported the numerical study to elaborate the characteristics of Robin's conditions for three-dimensional hydromagnetic Casson liquid flow past a bidirectionally moving surface. Nadeem et al. [19] provided the analytical solution for boundary layer flow of Casson fluid with magnetic field due to exponential shrinking sheet. Further Nadeem et al. [20] extended their work to three dimensional Casson fluid flows by incorporating nanoparticles. Using implicit finite-difference approximation method Iqbal et al. [21] analyzed the micropolar Casson fluid with the influence of inclined magnetic field. Mehmood et al. [22] addressed the internal heating role on Casson fluid model with micro-rotation. Impact of radiation, chemical reaction and slip effects on Casson fluid through a porous medium and addressed by Mabood et al. [23]. Singh and Dandapat [24] examined the four different types of nonlinear stretching velocities for thin film flow of Casson fluid.

Another important aspect of heat transport phenomenon which attained the special focus is called thermal radiation. The suitable knowledge of heat transfer via radiation is essential for the achievement of best quality products in industry. Several engineering processes include space vehicles, hypersonic flights, gas turbines, nuclear power plants etc. involve the phenomenon of

radiation. Nowadays, radiative heat transport has also role in the techniques of renewable energy. Various researches [25-37] have been done in literature to describe the mechanism of radiation. Having all the above important aspects in mind, here our plan is to elaborate the features of radiation in Casson liquid flow generated by stretched cylinder through the suspension of liquid-particles. We also utilized the concept of non-linear radiation phenomenon. The Robin's condition is accounted for convective heat transport at boundary of cylinder. Numerical computation is made to find the solution of non-linear governed expressions. Various authors in the literature used different and analytical techniques to find the solutions of different fluid flow problems [38-42]. The results of dimensionless quantities have been visualized for various values of emerging physical constraints.

Nomenclature

a	: Radius of the cylinder(m)
Bi	: Biot number
B_0	: Magnetic field
b	: Stretching rate
C_f	: Local skin-friction coefficient
c_m	: Specific heat of dust-particles(J/kgk)
c_p	: Specific heat of liquid(J/kgk)
Ec	: Eckert number
f	: Similarity variable for stream function
h	: Coefficient of convective heat transport
K	: Stokes resistance coefficient
k	: Thermal conductivity(W/mK)

Greek Symbols

β	: Casson parameter
β_1	: Parameter of liquid-particle interaction
θ	: Dimensionless temperature
θ_w	: Temperature heat ratio
μ	: Dynamic viscosity(kg/ms)
ν	: Kinematic viscosity(m^2/s)
ω	: Density ratio
η	: Similarity variable
γ	: Curvature parameter
ρ	: Liquid density(kg/m^3)
ρ_p	: Dust-particle density(kg/m^3)
τ	: Relaxation time of particle-phase

l	: Reference length	τ_T	: Time of thermal equilibrium
l^*	: Dust-particles mass concentration	τ_v	: Dust-particle relaxation time
m	: Dust-particle mass	Subscripts	
M	: Magnetic parameter	p	: Dust particles
N	: Number density of the particle phase	w	: At the wall
		∞	: In the free stream
Nu_x	: Local Nusselt number		
Pr	: Prandtl number		
q_r	: Heat flux of radiation		
R	: Parameter of radiation		
Re_x	: Reynolds number		
T_f	: Hot liquid temperature(K)		
U_w	: Stretching velocity		
z, r	: cylindrical coordinates(m)		

2. Formulation of the problem

We propose to elaborate the laminar flow of non-Newtonian Casson fluid by stretching hollow cylinderwith suspended particles. Thez-axis is along axis of the cylinder and r - axis normal it. Assumed that stretching surface of the velocity $U_w(z)$, surface temperature T_w and magnetic field of strength B_0 is exposed on r direction. Also assumed that cylinder is heated by convection from a hot fluid at temperature T_f itgives a heat transfer coefficient h_f . The size and shape of the dust particles is uniform and spherical. With all these assumption the governing equations are ([14],[43]):

Figure 1: Geometry of problem under investigation.

$$\frac{\partial(rw)}{\partial z} + \frac{\partial(ru)}{\partial z} = 0 \quad (1)$$

$$w \frac{\partial w}{\partial z} + u \frac{\partial w}{\partial r} = \nu \left(1 + \frac{1}{\beta}\right) \left(\frac{\partial^2 w}{\partial r^2} + \frac{1}{r} \frac{\partial w}{\partial r}\right) + \frac{KN}{\rho} (w_p - w) - \frac{\sigma B_0^2 w}{\rho}, \quad (2)$$

$$w_p \frac{\partial w_p}{\partial z} + u_p \frac{\partial w_p}{\partial r} = \frac{K}{m} (w - w_p), \quad (3)$$

$$w_p \frac{\partial u_p}{\partial z} + u_p \frac{\partial u_p}{\partial r} = \frac{K}{m} (u - u_p), \quad (4)$$

$$\frac{\partial(r\rho_p w_p)}{\partial z} + \frac{\partial(r\rho_p u_p)}{\partial r} = 0 \quad (5)$$

$$\rho c_p \left(w \frac{\partial T}{\partial z} + u \frac{\partial T}{\partial r}\right) = \frac{k}{r} \frac{\partial}{\partial r} \left(r \frac{\partial T}{\partial r}\right) + \frac{N c_p}{\tau_T} (T_p - T) + \frac{N}{\tau_v} (w_p - w)^2 - \frac{1}{r} \frac{\partial(rq_r)}{\partial r}, \quad (6)$$

$$w_p \frac{\partial T_p}{\partial z} + u_p \frac{\partial T_p}{\partial r} = -\frac{c_p}{\tau_T c_m} (T_p - T). \quad (7)$$

The boundary conditions can be defined as([5]):

$$w = U_w(z) = b \frac{z}{l}, \quad u = 0, \quad -k \frac{\partial T}{\partial r} = h(T_f - T) \text{ at } r = a$$

$$w \rightarrow 0, \quad w_p \rightarrow 0, \quad u_p \rightarrow u, \quad \rho_p \rightarrow \omega_p, \quad T = T_\infty, \quad T_p = T_\infty \text{ as } r \rightarrow \infty \quad (8)$$

where (w, u, T) and (w_p, u_p, T_p) are denotes components of velocity and temperature of fluid and dust particle respectively, ν for kinematic viscosity, ρ for fluid density, ρ_p for dust-particle density, K for Stoke's constant, m for thermal equilibrium at time, N for number density of dust particles, τ_v for relaxation time of ρ_p , τ_T for thermal equilibrium time and ω for density ratio.

In the expression (6) q_r is denoted by Rosseland approximation[43]:

$$q_r = -\frac{4\sigma^*}{3k} \frac{\partial T^4}{\partial r} = -\frac{16\sigma^*}{3k} T^3 \frac{\partial T}{\partial r}. \quad (9)$$

Here k^* for mean absorption coefficient, σ^* for Stefan-Boltzmann constant.

Dimensionless variables are defined as[5]:

$$\left. \begin{aligned} u &= -\frac{a}{r} \sqrt{\frac{\nu b}{l}} f(\eta), \quad w = U_w(z) f'(\eta), \quad \eta = \frac{r^2 - a^2}{2a} \sqrt{\frac{U_w}{\nu}}, \\ u_p &= \frac{a}{r} \sqrt{\frac{\nu b}{l}} F(\eta), \quad w_p = U_w(z) g(\eta), \quad \rho_r = H(\eta) \\ T &= T_\infty (1 + (\theta_w - 1)\theta), \quad T_p = \frac{T_p - T_\infty}{T_f - T_\infty}. \end{aligned} \right\} \quad (10)$$

with $\theta_w = \frac{T_f}{T_\infty}$, $\theta_w > 1$ being the temperature ratio parameter.

Applying equation (10) into equations (1)-(7), it reduces to the following forms

$$\begin{aligned} (1 + 2\eta\gamma) \left(1 + \frac{1}{\beta}\right) f''''(\eta) + 2\gamma f''(\eta) - (f'(\eta))^2 + f(\eta) f''(\eta) + \\ l^* \beta_1 H(\eta) (g(\eta) - f'(\eta)) - M f'(\eta) = 0, \end{aligned} \quad (11)$$

$$F(\eta) g'(\eta) - g^2(\eta) - \beta_1 (f'(\eta) - g(\eta)) = 0, \quad (12)$$

$$F(\eta) F''(\eta) - \left(1 + \frac{\gamma}{2\eta\gamma}\right) (F(\eta))^2 + \beta_1 [f'(\eta) + F(\eta)] = 0, \quad (14)$$

$$H(\eta) g(\eta) + F(\eta) H'(\eta) + H(\eta) F'(\eta) - \left(1 + \frac{\gamma}{2\eta\gamma}\right) H(\eta) F(\eta) = 0, \quad (15)$$

$$\begin{aligned} (1 + 2\eta\gamma) \left(1 + R \frac{d}{d\eta} (1 + (1 + \theta_w)\theta)^3\right) \theta''(\eta) + \text{Pr} [f(\eta)\theta(\eta) - 2f'(\eta)\theta(\eta)] \\ + 2\gamma\theta'(\eta) + \frac{NPr}{\rho\tau_T b} (\theta_p(\eta) - \theta(\eta)) + \frac{NPrEc}{\rho\tau_v} [g(\eta) - f'(\eta)]^2 = 0, \end{aligned} \quad (16)$$

$$2g(\eta)\theta_p(\eta) + F(\eta)\theta'_p(\eta) + \frac{c_p l}{\tau_T c_{mb}} (\theta_p(\eta) - \theta(\eta)) = 0. \quad (17)$$

The boundary conditions (9) become:

$$\begin{aligned} f(\eta) = 0, f'(\eta) = 1, \quad \theta'(0) = -Bi(1 - \theta(0)) \text{ at } \eta = 0, \\ f'(\eta) = 0, g(\eta) = 0, F(\eta) = -f(\eta), H(\eta) = \omega, \theta_p(\eta) = 0, \theta(\eta) = 0 \quad \text{as } \eta \rightarrow \infty, \end{aligned} \quad (18)$$

$\gamma = \sqrt{\frac{l\nu}{a^2}}$ for curvature parameter, $M = \frac{\sigma B_0^2 l}{\rho b}$ for magnetic parameter, $\beta_1 = \frac{l}{\tau b}$ for liquid-particle interaction parameter, $Pr = \frac{\mu c_p}{\rho}$ for Prandtl number, $R = \frac{16\sigma^* T_\infty^3}{3k^* k \rho c_p}$ for radiation parameter,

$Ec = \frac{bl^2}{c_p}$ for Eckert number, $l^* = \frac{mN}{\rho}$ for mass concentration dust particles and $Bi = \frac{h_f}{k} \sqrt{\frac{\nu}{b}}$ Biot number.

The skin friction coefficient and the Nusselt number can be obtained as

$$C_f = \frac{\mu \left(\frac{\partial u}{\partial r} \right)_{r=a}}{\rho U_w^2} \text{ and } Nu_x = - \frac{\mu \left(\frac{\partial u}{\partial r} \right)_{r=a}}{k(T_f - T_\infty)}.$$

Using the non-dimensional variables, we obtain

$$C_f Re_x^{\frac{1}{2}} = \left(1 + \frac{1}{\beta} \right) f''(0) \text{ and } \frac{Nu_x}{Re_x^{\frac{1}{2}}} = -[1 + R\theta_w^3] \theta'(0)$$

where $Re_x = \frac{U_w x}{\nu}$ is the local Reynold's number.

3. Result and Discussions

In this section, nonlinear ordinary equations (11) to (17) along with the corresponding boundary conditions (18) do not seem feasible solution. Firstly we separated the equations (11) to (17) with conditions (18) into a set a simultaneous ten first order differential equations. To obtained solution of these equations we required corresponding initial conditions but here the values of $f'(\eta)$, $\theta(\eta)$, $\theta_p(\eta)$, $g(\eta)$ and $F(\eta)$ are unknown as η tends to ∞ , so these missing conditions can be found using the shooting method by guessing the values of ∞ . Once we achieve the missing values called as fixed value apply the Runge-Kutta-Fehlberg integration scheme([7], [15]). The profiles of liquid velocity and liquid temperature for fluid and dust-phases are aforethought to research the influence of assorted flow dominant parameters. The numerical results of present model are matched with previous the available solutions and located to be sensible agreement as shown in table 1. From the tables 2-5, we can analyze the friction factor, Nusselt number, presence/absence of nonlinear thermal radiation also Newtonian and non-Newtonian behavior. The figures 2 and 3 are plotted to visualize the effects of Casson parameter(β) on velocity distribution for both phases. Figure 2 depicts that the increase in parameter of Casson leads to reduce the curves of velocity of both phases and hence the layer of thickness decreases. On contrast, an opposite response is observed for both liquid and dust phases temperature and its relevant layer of thickness (see figure 3).

Figures 4 and 5 describe the influences of curvature parameter (γ) on the profiles of velocity and temperature. From figure 4, one can observe that the curves of velocity are boost up for larger parameter of curvature. Moreover the liquid velocity within the vicinity of boundary layer is higher in the situations of cylinder in comparison to flat surface. The increment in cylinder diameter corresponds to lower profile of velocity within the layer of boundary. Figure 5 illustrate the impact of curvature parameter on temperature profile. Here the strengthening of curvature parameter sloping down the temperature profiles and corresponding thickness of layer. The behavior of the velocity for variation of magnetic parameter can be explored from figure 6. The increasing values of parameter of magnetic lead to a lower velocity profile. The central reason for this is an applied magnetic force normal to electrically-conducting liquid which has the ability to generate drag-like force named as Lorentz force. This force acts in direction opposite to that of flow which tends to impede its motion. The dimensionless temperature of both liquid and particle-phases is remarkably boost up for larger magnetic parameter which fully agrees with physical phenomena and can be seen in figure 7.

Figure 8 is drawn to see the impact of parameter of liquid-particle interaction β_1 on the velocity of both phases. It is clear from figure 8, for higher values of parameter of liquid-particle interaction lead to enhance the velocity of dust-phase while an opposite trend is obtained for velocity of liquid-phase. A friction factor is generated in liquid due to consideration of dust-particles which retards the flow. Figure 9 elucidates the effect of parameter of liquid-particle interaction on temperature profile of both liquid and particle-phases. It shows the decreasing trend over the dimensionless temperature. Figure 10 elaborates the variations of temperature for several values of Biot number. We can observe from this plot, an increase in the Biot number gives rise to the enhancement in temperature profile of both phases. This result qualitatively

agrees with expectations, because the coefficient of heat transport enhanced for higher Biot number which is responsible for an increase in temperature.

Figure 11 exhibits the effect of Eckert number on temperature profile of the fluid and particle phase. It shows that, the increasing trend over the dimensionless temperature. The central reason for this change is that the viscosity of liquid gains energy from liquid motion and convert it into internal energy due to which liquid temperature is heated. Figure 12 is plotted to visualize the effects of radiation on temperature profile of both phases. The above graphs elucidate that, the temperature profile and corresponding thermal boundary layers of both fluid and dust phase increases by increasing the parameter of radiation. The presence of parameter of radiation provides more heat to liquid that give rise to temperature. The temperature of the fluid much more pronounced in non-linearized thermal radiation case than that of compared to linearized thermal radiation case its observed from table 2. Figure 13 presents the impacts of parameter of temperature ratio (θ_w) on liquid temperature. As expected, the increment in ratio parameter corresponds to higher temperature of both liquid and dust-phases. The ratio of momentum and thermal diffusivities is the definition of Prandtl number. The weaker thermal-diffusion is obtained in the case of higher Prandtl number that produces a reduction in temperature of both liquid and dust-phases (see figure 14).

Table 1: Comparison of the results for the dimensionless temperature gradient $\theta'(0)$ for various values of Pr in the case of $\beta = 0$, $Ec = 0$ and $\beta_1 = 0$.

Pr	$-\theta'(0)$	
	1	10
Grubka and Bobba [35]	-1.3333	4.7969
Ali [30]	-1.3333	4.7969
Abel et al. [37]	-1.3333	4.7969
Present result	-1.33332	4.79672

Table 2: Numerical values of skin friction coefficient and Nusselt number for different values physical parameters.

γ	M	β	β_1	$-\left(1+\frac{1}{\beta}\right)f''(0)$	$-[1+R\theta_w]\theta'(0)$
0				2.000003	1.340784
0.2				2.027095	1.338303
0.4				2.053544	1.335819
	0			1.416673	1.338935
	1			1.828354	1.340438
	2			2.163083	1.340387
		0.5		2.994117	1.338365
		1		2.448664	1.339959
		1.5		2.237015	1.340373
			1	2.002742	1.340537
			2	2.057506	1.461928
			3	2.084342	1.518296

Table 3: Numerical values of Nusselt number for different values physical parameters.

Bi	Ec	Pr	R	θ_w	$-[1+R\theta_w]\theta'(0)$
1					1.340537
2					2.159097
3					2.700733
	0.5				1.340537
	1				1.248385
	1.5				1.156768
		4			1.303165
		5			1.340537
		6			1.368548
			0		0.755726
			0.5		1.340537
			1		1.879962
				1.1	1.346472
				1.2	1.340537
				1.3	1.334213

Table 4: Numerical values of Nusselt number for linear and nonlinear radiation with different values physical parameters.

Bi	Ec	γ	Pr	R	β_1	$-[1 + R\theta_w]\theta'(0)$	
						Non linear radiation	Linear radiation
1						1.340537	0.732318
2						2.159097	1.203488
3						2.700733	1.532061
	0.5					1.340537	0.732318
	1					1.248385	0.68163
	1.5					1.156768	0.630942
		0				1.340784	0.732405
		0.2				1.338303	0.730627
		0.4				1.335819	0.728851
			4			1.303165	0.713963
			5			1.340537	0.732318
			6			1.368548	0.746081
				0		0.755726	0.755726
				0.5		1.340537	0.712351
				1		1.879962	0.679036
					1	1.340537	0.732318
					2	1.461928	0.795735
					3	1.518296	0.82462

Table 5: Numerical values of skin friction coefficient for ($\beta = 0$) Newtonian fluid and ($\beta = 1$) nonNewtonian fluid.

γ	M	β_1	$-\left(1 + \frac{1}{\beta}\right)f''(0)$	
			Non Newtonian fluid	Newtonian fluid
0			2.000003	1.732051
0.2			2.027095	1.777126
0.4			2.053544	1.821301
	0		1.416673	1.228832
	1		1.828354	1.585583
	2		2.163083	1.875453
		1	2.002742	1.736602
		2	2.057506	1.784034
		3	2.084342	1.807279

Figure 2: Velocity curves for different β .

Figure 3: Temperature curves for different β .

Figure 4: Velocity curves for different γ . Figure 5: Temperature curves for different γ .

Figure 6: Velocity curves for different M .

Figure 7: Temperature curves for different M .

Figure 8: Velocity curves for different β_1 . Figure 9: Temperature curves for different β_1 .

Figure 10: Temperature curves for different Bi .

Figure 11: Temperature curves for different Ec .

Figure 12: Temperature curves for different θ_w . Figure 13: Temperature curves for different R .

Figure 14: Temperature curves for different values Pr .

4. Conclusion

This work has great importance in the field of science and technological. The considered problem is quite useful in guided missiles rain erosion, fluidization, atmospheric fallout, paint and aerosol spraying, lunar ash flows and cooling of nuclear reactor. Here we explored the impact of nonlinear thermal radiation on flow and heat transfer of Casson fluid over a stretching hollow cylinder in the presence of fluid-particle suspension and convective boundary condition. Some important features regarding various physical constraints on different flow quantities of the problem are follows:

- The rising values of Casson and magnetic parameter improves the temperature profiles of the flow.
- The factor of friction reduced for larger parameter of liquid-particle interaction due to which rate of heat transport is improved.

- The thickness of thermal layer is weaker when the Prandtl number increases. The utilization of proper Prandtl number has pivotal importance in the processes of industrial products.
- The temperature is enhanced significantly by the use of larger radiation and temperature ratio parameters.
- The fluid and dusty phase of temperature profile increase rapidly for increasing values of Biot number and Eckert number.

This work can be further extended for various models of non-Newtonian liquids like differential, integral and rate type models. Also this research can be extended for various geometries and different physical aspects. This work will serve as a basis for future research progress in field of dusty fluid.

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